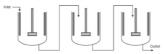
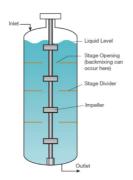
Continuous Flow Reactor

I deal continuous flow reactors are generally considered to be either plug flow or backenized. The closest physical embodiment of a plug flow reactor is a Static Mixer® unit in a pipe. However, the very high cost of such construction per unit of reactor volume makes its use cost-prohibitive for all but very short retention time applications.

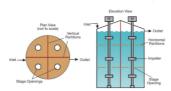
More commonly, a backmixed reactor is used. To reduce retention time required, and thus total reactor volume, usually there are multiple stages used. The simplest embodiment of a backmixed reactor is an



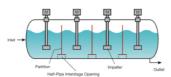
The above arrangement requires one agitator and one tank for each stage. It is possible to reduce capital and operating costs by compartmentalizing a single vessel, allowing the use of one agitator with multiple impellors. This arrangement is often referred to as an agitated column:



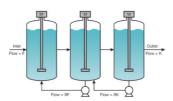
Very large tanks can be compartmentalized both horizontally and vertically



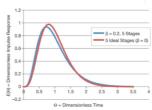
Horizontal tanks can be compartmentalized as use



Many other configurations are possible. All reduce capital and operating costs compared to discreet tasks is neises. However, all such arrangements permit a certain amount of backming between stages, which reduces stage referency. A key neumous of reduceming is colled the backmin ratio, by, which is the ratio of backming to foot backming the other staged reactor with backmining is to true it as lad to backmin flow to process food flow. A good way to model a staged reactor with backmining is to true it as lad to backmin flow some flow with recycle between the some process.



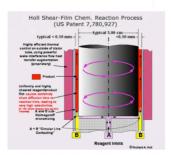
Backmixing affects residence time distribution (RTD) and reaction conversion. An illustration of the effect of backmixing on RTD is shown below, comparing 5 ideal stages to 5 stages with a backmix ratio (B) of 0.2:



Balancing the mixing and the backmixing in such designs is the key to success in continuous flo

The previous internations are coursely of Chemical Engineering Progress, and were used in part in "Designing Multistage Agitated Reactors", G. Benz, Chemical Engineering Progress, January 2014, p. 30-36.

If your reaction is fast but is heat or mass transfer limited, or is selective, a novel reactor scheme should be considered. It consists of blending with a shear film in Counter flow. Reaction speed and conversion are very high compared to conventional reactor design for fast reactions. The basic elements are shown below.



Benztech is a representative of the manufacturer of the above equipment, Holl Partners, LLC. Contact us to see if your reaction would be a good candidate for such a system